**Original Research** 

# *Enterococcus faecalis* Bioflocculant Enhances Recovery of Graphene Oxide from Water

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> Received: 12 September 2017 Accepted: 17 December 2017

### Abstract

Bioflocculation is a promising method of removing GO from the water as it is safe, biodegradable, and non-secondary pollution, but few studies on effective and economic bioflocculant of GO have been reported. Accordingly, this work evaluated flocculation efficiency of an extracellular bioflocculant named MBF-21 produced by *Enterococcus faecalis*. Optimum culture conditions for bioflocculant production were initial medium pH of 7 and incubation temperature of 40°C. The optimum carbon and nitrogen sources for bioflocculant production were glucose and beef extract. Results of Fourier transform infrared (FTIR) indicated the presence of carboxyl, hydroxyl, and amide groups on the MBF-21. The Zeta potential of MBF-21 analysis revealed that MBF-21 was mainly negatively charged. MBF-21 showed a significant ability in flocculation of GO, and flocculation efficiency was over 90% under neutral, acidic, and alkaline conditions, indicating that flocculation of GO was ion-independent. The conditions for flocculation of GO were optimized by response surface methodology (RSM) and determined to be an 11.57 mg/L dose and flocculation time of 75 min.

**Keywords**: bioflocculant, *enterococcus faecalis*, graphene oxide, microbial flocculation, response surface methodology

### Introduction

Graphene oxide (GO) has been widely used in electronics, biosensors, pipes, and semiconductors for its excellent electrochemical properties [1]. In recent years, with the wide use of GO, wastewater containing GO are increasingly discharged. According to previous studies, GO can negatively impact wastewater microbial communities [2-3] because GO can hinder the essential microbial functions in activated sludge processes [4-5]. Furthermore, the presence of GO in activated sludge may lead to the decline in BOD<sub>5</sub> and depress the removal of nitrogen and phosphorus in the biological treatment process [6].

The methods of bioflocculant for treatment of GO in the water are popular for its safety, biodegradability, and non-secondary pollution. Bioflocculant is an extracellular biopolymer derived from the natural secretions of bacteria [7]. As the predominant components of bioflocculant are polysaccharide, glycoprotein, protein, and nucleic acid, bioflocculation is becoming a popular method for water treatment [8]. Although studies have reported

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on the removal of GO from water with bioflocculation, research in this area is still limited [9]. It is well known that influence factors, temperature, and pH are major factors in controlling the bioflocculation process, whereas bioflocculant dosage and flocculation time need further study before the practical application for the removal of GO by biofloccuant.

Accordingly, the major objectives of this research are to: (1) screen and identify a novel bioflocculant-producing strain from active sludge; (2) study various factors affecting bioflocculant production, including carbon source, nitrogen source, initial pH, and temperature of incubation; (3) evaluate and optimize the effects of temperature, pH, bioflocculant dosage, and flocculation time by response surface methodology; and (4) explore mechanisms of flocculation of GO with bioflocculant.

# **Material and Methods**

## Identifying Bioflocculant-Producing Strains

The morphological character of the selected strain was observed with a Nikon E100 microscope and the physiological and biochemical characteristics were identified by Bergey's Manual of Systematic Bacteriology. PCR amplification of 16S rDNA was identified with Sangon Biotechnology (Shanghai, China Co., Ltd).

## Culture Mediums for Bioflocculant Production

The selected strain was cultivated using nutrient broth containing 5 g/L of peptone, 1.5 of g/L beef extract, 1.5 g/L of yeast extract, and 5 g/L of NaCl. PT-1 culture was used as bioflocculant subculture. The composition of the bioflocculant production medium PT-1 were as follows: glucose, 20 g/L; yeast extract, 0.5 g/L; urea, 0.5 g/L; K<sub>2</sub>HPO<sub>4</sub>, 5 g/L; KH<sub>2</sub>PO<sub>4</sub>, 2 g/L; MgSO<sub>4</sub>, 0.2 g/L; and NaCl, 0.1 g/L. The initial pH of the medium was adjusted to 7.0-7.2. After sterilization and inoculation, the strains were cultured at 30°C in a rotary shaker at 150 rpm for 72h. Five factors (carbon source, nitrogen source, initial pH, temperature, and incubation period) were investigated for optimizing the culture conditions for the strain *Enterococcus faecalis*. To determine the effect of the carbon and nitrogen sources on bioflocculant production, glucose was replaced with sucrose, fructose, lactose, starch, and maltose (20 g/L for each type of compounds), respectively, and peptone was replaced with  $(NH_4)_2SO_4$ ,  $NH_4NO_3$ ,  $NaNO_3$ , beef extract, and urea (3 mg/L for each type of compound) separately. Since our preliminary experiments show that the synthesis and growth process of microbial flocculant is synchronized, the compounds added the same quality here, just by changing the flocculation efficiency directly shows the optimal medium for synthesis of flocculant. All the compounds used in our culture are analytically pure. Initially, the pH of the production media was adjusted to 15-50°C. The effect of the time course of bioflocculant production was investigated between 0 and 96 h. All the analyses were conducted in triplicate.

#### Preparing MBF-21

The selected strain was inoculated into a 150-ml flask containing 50 ml T-1 medium. The bioflocculant produced by selected strain was termed MBF-21. MBF-21 was produced by shaking the flask under 30°C at 150 rpm for 72 h. Cell-free supernatant was obtained by centrifuging at 7,000 rpm for 30 min. The method of the bioflocculant purification in this study was according to previous studies [10-11]. Two volumes of cold ethanol (at 4°C) were added to 1 L culture broth. After centrifuging at 8,000 rpm for 30 min, the obtained precipitate was dissolved in 100 ml deionized water by stirring, and adding 50 mL of 2% cetylpyridinium chloride (CPC) solution. After 3 h, the precipitate was collected and dissolved in 100 ml of 0.5 M NaCl solution. Two volumes of cold ethanol were then added to obtain the precipitate, which was washed with ethanol and dissolved in 5 mL of deionized water and vacuumdried. About 1.2 g of pure MBF-21 was obtained in 1L culture broth.

## Batch Experiment of Bioflocculation of GO

GO was diluted to 60 mg/L by the addition of distilled water for stock solution. The effects of flocculation conditions (temperature, pH, flocculation time, and bioflocculant dosage) were studied. The pH was adjusted to approximately 3.0-11.0 by 0.1 M HCl and 0.1 M NaOH. Likewise, the effects of temperature were incubated at desired temperatures.

Table 1. Independent variables and their levels in the experimental design.

Independent verichles	Symbols	Code levels					
independent variables		-2	-1	0	+1	+2	
Temperature (°C)	A	0	10	20	30	40	
pH	В	3	5	7	9	11	
Bioflocculant dosage (mg/L)	С	0	4	8	12	16	
Flocculation time (min)	D	0	25	50	75	100	

After setting up of fixed parameters, tubes containing the mixture of GO solution and MBF-21 were shaken in an orbital shaker (Model-HZQ-X100, HDL APPARATUS Ltd., China) and stirred at a constant speed of 250 rpm. The initial GO concentration was determined under optical density of 290 nm (OD<sub>290</sub>) by a UV-VIS Spectrophotometer (Model-T6, PGENERAL Ltd., China). The optical density of the supernatant was determined at half height of the clarified culture. Culture broth without bioflocculant was used as control. Flocculation efficiency of GO was calculated by Equation (1) [12-16]:

Flocculation Efficiency (%) = 
$$(A - B)/A \times 100$$
(1)

...where A is  $OD_{290}$  value of sample and B is  $OD_{290}$  value of control.

#### Optimizing Flocculation of GO with MBF-21

Design Expert Software (version 8.0) was used for statistical design of the experiments and data analysis. In this study, the central composite design (CCD) and response surface methodology (RSM) were applied to optimize the four factors: MBF-21 dosage, temperature, flocculation time, and pH. The narrower ranges of MBF-21 dosage, temperature, flocculation time, and pH. The narrower ranges of MBF-21 dosage, temperature, flocculation time, and pH were determined prior to designing the experimental runs. The narrower ranges of MBF-21 dosage, flocculation time, temperature, and pH were chosen: 0-16 mg/L, 0-100 min, 0-40°C, and 3–11, respectively. The 4 independent factors with 5 different levels (-2, -1, 0, +1, +2) were investigated and the experimental designs are shown in Table. 1.

The response variable (y) for flocculation efficiency was fitted by a second-order model and calculated by the following quadratic polynomial equation (2):

Flocculation Efficiency =+71.53 - 4.66 \* A  
+ 0.43 \* B + 22.49 \* C + 18.06\*D + 2.67\*A  
\* B + 0.86 \* A \* C - 2.95 \* A \* D - 0.98\*  
B \* C - 0.96 \* B \* D + 8.96 \* C \* D - 5.74  
\* 
$$A^2$$
 - 1.68 \*  $B^2$  - 9.73 \*  $C^2$ -9.94 \*  $D^2$   
(2)

...where flocculation efficiency is the predicted response and the independent factors *A*, *B*, *C*, and *D* are temperature, pH, MBF-21 dosage, and flocculation time, respectively. All the analyses were conducted in triplicate. The error bars are marked in all the figures except the central composite design (CCD), and response surface methodology (RSM) data analysis. The data in the response surface are fitted with the average of three sets of repeated data and they were analyzed by ANOVA.

#### Analytical Methods

Zeta potential measurement of MBF-21 was conducted by Zeta potential analyzer (Malvern nano ZS, Malvern, England). A Fourier-transform infrared spectrometer (Nicolet 6700, ThermoFisher, USA) was used for space atmospheric component detection of MBF-21. A scanning electron microscope (XL30-ESEM, FEI, USA) was applied to detect flocculated GO.

#### **Results and Discussion**

# Screen and Identification of Bioflocculant-Producing Strain

Strains were isolated from activated sludge of a Second Wastewater Treatment Plant, Changchun, China. Seven strains with flocculation efficiency greater than 80% for 30 mg/L GO suspension were screened and identified. Among the 7 strains, strain N-21 was rod-shaped, gram-positive, unmotile, catalase-negative, arginine dihydrolase-positive, and oxidase-negative, and produced acids from glucose under anaerobic conditions. The 16S rDNA was sequenced after polymerase chain reaction (PCR) amplification and compared with sequences deposited in databases. A total of 1,501 bp of 16S rDNA of N-21 was determined. The highest level of 16S rDNA sequence is 99.9% – similar to *Enterococcus faecalis* (NCBI EU285587).



Fig. 1. Zeta potential of MBF-21 and its Fourier-transform infrared spectrometer analysis: a) Zeta potential of purified MBF-21, b) infrared radiation (IR) spectrum investigated of purified MBF-21.

a) 100

Flocculation efficiency (%)

90

80

70 60

50 40

30 20

10

b)100

Flocculation efficiency (%)

90

80

70

60 50

40 30

20 10

0

Urea

# Zeta Potential of MBF-21 and its Fourier-Fransform Infrared Spectrometer Analysis

The microbial flocculant of *Enterococcus faecalis*, termed MBF-21, was purified and its infrared radiation (IR) spectrum was investigated. The IR spectrum of the purified MBF-21 exhibited an amide band broad hydroxyl stretching peak at 3,430 cm<sup>-1</sup>, and a carboxyl band at 1,641-1,497 cm<sup>-1</sup> as presented in Fig. 1a). The adsorption peak at 3,006-2,924 cm<sup>-1</sup> indicated the C-H stretching vibration. Strong adsorption peaks present in the range 1,024 cm<sup>-1</sup> are typical characteristics for sugar derivatives [17]. Zeta potential measurement of MBF-21, (Fig. 1b), indicated that MBF-21 was negatively charged in both alkaline and acidic solutions.

# Effects of Carbon and Nitrogen and Sources on MBF-21 Production

The effects of various carbon sources on the production of MBF-21 were evaluated. As shown in Fig. 2a), lactose, fructose, and glucose were favorable carbon sources for both the production of MBF-21 and cell growth. The glucose as carbon source was the cheapest and achieved the highest flocculation rate

Glucose Lactose Fructose Sucrose Maltose Starch Carbon sources

Flocculating activity(%)

Flocculation efficiency (%)

Biomass dry weight (g/L)

(NH<sub>4</sub>)<sub>2</sub>NO<sub>3</sub> (NH<sub>4</sub>)<sub>2</sub>Cl<sub>4</sub> (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub>

Biomass (g/L)

15

12

9

6

3

15

12

Biomass dry weight (g/L)

a) 100

Flocculation efficiency

Fig. 2. Effect of carbon sources and nitrogen sources on *Enterococcus faecalis* and production of MBF-21: a) effect of carbon sources on MBF-21 production with peptone used in the medium as nitrogen source and b) the effect of nitrogen sources on MBF-21 production with glucose used in the medium as carbon resource.

Nitrogen sources

Beef

extract

Peptone

15

of 94.7%, thus the glucose was selected as the carbon source in the flocculation of GO. Glucose was also reported as the favorable carbon source in the production of bioflocculant [18]. Fig. 2b) illustrates the effects of different nitrogen sources on the production of MBF-21, when glucose was used as the carbon source. The results showed that all inorganic nitrogen sources led to poor production of MBF-21 and cell growth, and the organic nitrogen sources were evidently better than inorganic nitrogen sources for MBF-21 production. Beef extract was therefore selected as the nitrogen source in the following experiments. Organic nitrogen sources were also reported as the favorable carbon sources in the production of bioflocculant [19].

# Effect of Initial pH and Temperature on MBF-21 Production

The effect of the initial pH in fermentation runs on the cell growth and flocculating activity were examined (Fig. 3a). The initial pH of the culture medium could affect the electrification state of strain cell and redox potential, and enzymatic reaction of bioflocculantproducing strains. The highest flocculating rate was recorded between 6 and 7, and the biomass (dry weight)



Fig. 3. Effect of initial pH and temperature on *Enterococcus faecalis* and production of MBF-21: a) effect of initial pH on MBF-21 production and b) effect of temperature on MBF-21 production.



Fig. 4. Time course of the production of MBF-21; rrror bars indicate standard deviation of triplicate experiments.

was highest at pH 6. Fig. 3b) illustrates the effect of culture temperature on fermentation runs. The cultures grown at 35°C and above the culture temperature showed a rise in flocculating rate, reaching 94.77 % at 40°C.

# Time Course of the Production of MBF-21

The growth curve of *Enterococcus faecalis* and the flocculating activity of the culture broth are shown in Fig. 4. During fermentation, the production of MBF-21 paralleled the growth of the biomass. The flocculating activity in different culture supernatants from early stationary cultures was the highest (93.28% at 60 h). The same phenomenon was reported in the cultivation of *Aspergillus parasiticus* [18], *Bacillus mucilaginosus* [20], and *Citrobacter* sp. TKF04 [21]. At late stationary phase, the flocculating activity stopped increasing, which may have been due to the activities of enzymes that were up to maximum value [22]. After 72 h, *Enterococcus faecalis* reached its early dead phase, and consequently the flocculating activity of MBF-21 remained the same.

# Optimizing Flocculation of GO using RSM Effects of MBF-21 Dosage, Temperature, pH, and Flocculation Time on Flocculation Efficiency

The experiment assignment and the collected response data are shown in Table 2. As shown in Table 3, the linear terms for flocculant dosage (C) and flocculation time (D) had significant effects on flocculation efficiency (F value < 0.05), but temperature (A) and pH (B) had no significant effects on efficiency. The relationship between temperature in the range of 10-40°C and flocculation efficiency was studied. Fig. 5 shows that the highest flocculation efficiency was achieved at 17.58°C. With the temperature raising from 10 to 17.58°C, flocculation efficiency increased from 69.87% to 71.81% and decreased to 60.72%, with temperature rising to 30°C.

Table 2. Experimental design and results of the central composite design.

Run		·			
	<sup>d</sup> T (°C)	pН	<sup>b</sup> BS (mg)	°FT (min)	°FA (%)
1	20.00	11.00	8.00	50.00	86.58
2	40.00	7.00	8.00	50.00	52.15
3	20.00	7.00	8.00	50.00	70.94
4	20.00	3.00	8.00	50.00	76.07
5	20.00	7.00	8.00	50.00	70.32
6	10.00	9.00	4.00	25.00	12.26
7	10.00	9.00	12.00	25.00	22.25
8	20.00	7.00	16.00	50.00	98.22
9	30.00	9.00	12.00	25.00	43.83
10	10.00	9.00	12.00	75.00	84.96
11	30.00	9.00	12.00	75.00	73.02
12	20.00	7.00	8.00	50.00	72.72
13	10.00	5.00	12.00	75.00	93.35
14	10.00	9.00	4.00	75.00	26.95
15	0.00	7.00	8.00	50.00	78.02
16	20.00	7.00	8.00	50.00	72.14
17	10.00	5.00	4.00	75.00	26.6
18	20.00	7.00	0.00	50.00	0.07
19	30.00	5.00	4.00	75.00	16.13
20	10.00	5.00	4.00	25.00	11.5
21	10.00	5.00	12.00	25.00	41.62
22	30.00	5.00	4.00	25.00	3.36
23	30.00	5.00	12.00	25.00	26.78
24	20.00	7.00	8.00	0.00	0.20
25	20.00	7.00	8.00	50.00	71.55
26	30.00	5.00	12.00	75.00	75.44
27	20.00	7.00	8.00	50.00	71.52
28	30.00	9.00	4.00	25.00	7.29
29	30.00	9.00	4.00	75.00	13.62
30	20.00	7.00	8.00	100.00	96.38

<sup>a</sup>Flocculational activity

<sup>b</sup>Bioflocculant size

°Flocculation time

<sup>d</sup>Temperature

Table 3 and Fig. 5 (above) show that the influence of pH on flocculation was not significant, and that flocculation efficiency just increased by 1%, with pH raising from 5 to 9. As shown in Figure 1 (above), Zeta potential measurement of MBF-21 illustrated that MBF-21 was mainly negatively charged in alkaline

Source	Sum of squares	DF	Mean square	F value	P Value
Model	27065.89	14	1933.28	7.03	0.0003
C-Flo dosage	12142.80	1	12142.80	44.13	< 0.0001
D-Flo time	7831.54	1	7831.54	28.46	< 0.0001
CD	1285.22	1	1285.22	4.67	0.0473
C^2	2594.63	1	2594.63	9.43	0.0078
D^2	2709.93	1	2709.93	9.85	0.0068
Residual	4127.21	15	275.15		
Lack of Fit	4123.61	10	412.36	572.58	< 0.0001
Pure Error	3.60	5	0.72		
R-Squared	0.8677				
Adj R-Squared	0.7442				
Adeq Precision	9.996				

Table 3. ANOVA analysis for responses Y (flocculation efficiency, %).

and acidic conditions. GO has been reported to have different electrical states at different pH – positively charged in acidic conditions (pH below 4) and negatively

4) [23-24]. So it could be concluded that electrostatic repulsion effect was not the main factor affecting flocculation efficiency.



charged in neutral and alkaline conditions (pH above

Fig. 5. Effect of 4 single variables on removal efficiency, including: a) temperature, b) pH, c) MBF-21 dosage (G value was 0 s<sup>-1</sup>), and d) flocculation time;  $\blacksquare$  is verified GO flocculation efficiency under selected conditions.



Fig. 6. Surface responses and contour plots showing interactive effect of selected variables on flocculation efficiency (grey spot on the response surface is the best point).

# Interaction between Flocculation Time and MBF-21 Dosage on Flocculation Efficiency

Table 3 shows that flocculation time (C) and MBF-21 dosage (D) were significant impact factors on flocculation efficiency. By changing the other two variables within their experimental ranges and keeping other variable values at middle levels, RSM provided the response surfaces and the contour plots for studying the interactions between the parameters and flocculation efficiency. As shown in Fig. 5 (above), at fixed pH and temperature, flocculation efficiency increased from 38.91% to 83.46% with the rise of dosage from 4 to 12 mg/L. At a fixed MBF-21 dosage of 8 mg/L, flocculation efficiency increased from 43.48% to 79.45% with time extension from 25 to 75 min. Lower dosage of 12 mg/L induced higher efficiency of over 80%. MBF-21 as a long-chain biopolymer performs bridging between GO particles as shown in Fig. 7b. When MBF-21 is insufficient, the bridging phenomena do not



Fig. 7. a) Scanning electron microscope of graphene oxide, b) scanning electron microscope of graphene oxide flocculated by MBF-21, c) scanning electron microscope of graphene oxide separated from MBF-21, and d) molecular structure of GO.

	Variables				<sup>h</sup> EF(%)			
No.	<sup>a</sup> T (°C)	рН	<sup>b</sup> FT (min)	° BS (mg)	<sup>d</sup> PV	° OV	f SD	
1	25	7	75	11.57	95.12	93.85	±0.90	
2	20	7	75	11.57	99.98	97.68	±1.63	
3	20	6	70	11.57	100.26	98.12	±1.51	
4	25	6.5	70	11.57	93.65	94.34	±0.49	
5	15	8	70	11.57	98.38	97.19	±0.84	

Table 4. Verification experiments at optimum conditions.

<sup>a</sup>Temperature

<sup>b</sup>Flocculation time

°Bioflocculant size

<sup>d</sup>Predicted values

<sup>e</sup>Observed values

fStandard deviation

<sup>h</sup>Flocculation efficiency

effectively form. Hummers chemical reduction method is considered to be one of the most efficient, economical, and highly efficient methods for synthesizing graphene. As intermediates in the preparation of graphene with Hummers method, GO still maintains a layered structure of graphite, whose containing groups include carboxyl, hydroxyl, epoxy, etc. (Figs 7a, d). These oxygen functional groups make GO have good dispersibility in water. The obtained GO with recovery methods used in this study maintained consistent water solubility and physical properties (Figure 7c).

GO contains abundant oxygen-containing functional groups on its large surface, such as hydroxyl, carboxyl, and epoxy groups, which makes it extremely hydrophilic in aqueous environments (Fig. 7d). For this reason, the change of pH cannot change the electrostatic adsorption in the flocculation process. And for the same reason, pH was not a significant factor on flocculation efficiency as shown in Fig. 5b). In the flocculation process, net trapping is the main factor in the flocculation mechanism as shown in Fig. 7b) [25-26].

# ANOVA Analysis and Certification for Response Surface Quadratic Model

The experimental data of flocculation efficiency were analyzed by ANOVA. All the factors followed secondorder effects, yielding a quadratic model for flocculation efficiency. The significance of each model term was determined by p-values (probability). A p-value less than 0.05 indicates that the model term is important and the insignificant terms (p-value > 0.05) are removed from final expression of the model [27]. In order to bind the response for Y (removal efficiency) to 100%, LOGIT transformation was used with upper limit as 100. The model, in terms of the coded factors of the flocculation process, was expressed as Equation (2). This model could adequately describe the response based on the p-value < 0.0001, which is far less than 0.05. Adequate precision evaluates the ratios of signal and noise ratio and a ratio greater than 4 is desirable [28]. The ratio was 9.996, demonstrating that this model could precisely describe the process (Table 3). Furthermore, the lack of fit value was insignificant relative to pure error as the p-value was less than 0.05. The value of correlation coefficient (R<sup>2</sup>) obtained in the present study was 0.884, which was close to  $R^2$  adj (0.74), indicating good agreement between the predicted and observed values of the experiments [29]. Therefore, it was a suitable model to predict flocculation efficiency of GO. Our study showed that temperature (A) and pH (B) were not significant factors on flocculation efficiency (Figs 5a and b). Their p-value was larger than 0.05 (data not shown in Table 3). At the same time, ANOVA analysis with the response surface quadratic model also proved that flocculation efficiency does not change with the change of these 2 factors viz temperature (A) and pH (B), that p-value was less than 0.05 (Table 3). For these reasons, we chose the most conventional condition viz pH 6.5-8 and temperature 15-25°C in the optimized experimental conditions [30]. According to the experimental results, the main factors affecting flocculation efficiency are flocculant dosage (C) and flocculation time (D).

The optimization of the operating conditions were conducted by the quadratic models of the experimental design [31-36]. In order to maximize flocculation efficiency and determine the effects of the flocculation process of GO, 5 optimum solutions labelled 1-5 provided by the models were selected and verified under selected optimum conditions. Table 4 illustrates that all the selected optimum solutions had desired prediction of flocculation efficiency with the maximum experimental data. By triplicates of the experiments, the validated experimental results of flocculation efficiency and the values predicted by the models are shown in Table 4. The observed values of flocculation efficiency ranging from 93.85% to 98.12% were desirable. The deviations between the experimental and predicted values ranged from 0.49% to 1.63%. Therefore, the model was considered to fit the experimental data very well.

# Conclusions

The results showed that *Enterococcus faecalis* produced bioflocculant that had never before been reported. The most preferred carbon and nitrogen sources for strain *Enterococcus faecalis* were glucose and beef extract, respectively. Fourier transform infrared (FTIR) indicated the presence of the carboxyl, hydroxyl, and C-H groups, which are typical characteristics for sugar moieties. The Zeta potential of MBF-21 analysis revealed that MBF-21 was mainly negatively charged. MBF-21 showed a high flocculation efficiency of GO without cations. Flocculation conditions of GO were optimized using response surface methodology. The results showed that highest flocculation efficiency over 98% occurred under optimistic conditions in which the dosage was

11.57 mg/L and flocculation time was 75 minutes. While temperature and pH are not significant factors in the flocculation process of GO, it was suggested that MBF-21 possessed excellent ability in flocculating GO from water.

# Acknowledgements

This work was supported by the National Natural Science Foundation of China (No. 51708248), the "13<sup>th</sup> Five-Year" Planning Project of Education Department of Jilin Province (2015, No. 438), and as a Major Project of Jilin Institute of Chemical Technology (No. 2015004).

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